



(19)

Europäisches Patentamt

European Patent Office

Office européen des brevets



(11)

EP 0 969 043 A1

(12)

EUROPEAN PATENT APPLICATION

(43) Date of publication:

05.01.2000 Bulletin 2000/01

(51) Int. Cl.⁷: C08L 23/10, C08L 21/00

(21) Application number: 99112169.0

(22) Date of filing: 24.06.1999

(84) Designated Contracting States:

AT BE CH CY DE DK ES FI FR GB GR IE IT LI LU
MC NL PT SE

Designated Extension States:

AL LT LV MK RO SI

(30) Priority: 01.07.1998 US 108492

(71) Applicants:

- Advanced Elastomer Systems, L.P.
Akron, Ohio 44311-1059 (US)
- EXXON CHEMICAL PATENTS INC.
Baytown, TX 77520-5200 (US)

(72) Inventors:

- Finerman, Terry
Akron, Ohio 44333 (US)

• Ellul, Maria D.

Silver Lake Village, Ohio 44224 (US)

• Abdou-Sabet, Sabet

Akron, Ohio 44313 (US)

• Datta, Sudhin

Houston, Texas 77019 (US)

• Gadkarl, Avi

Houston, Texas 77019 (US)

(74) Representative:

Weber, Thomas, Dr.Dipl.-Chem. et al
Patentanwälte
von Kreisler-Setling-Werner,
Postfach 10 22 41
50462 Köln (DE)

(54) Modification of thermoplastic vulcanizates using random propylene copolymers

(57) Random propylene thermoplastic copolymers can be used to increase the elongation to break and toughness of thermoplastic vulcanizates. Semi-crystalline polypropylene is a preferred thermoplastic phase. The rubber can be olefinic rubbers. Random thermoplastic polypropylene copolymers are different from conventional Ziegler-Natta propylene copolymers as the compositional heterogeneity of the copolymer is greater with Ziegler-Natta copolymers. This difference results in substantial differences in properties (elongation to break and toughness) between thermoplastic vulcanizates modified with random thermoplastic propylene copolymers and those modified with conventional Ziegler-Natta propylene copolymers. An increase in elongation to break results in greater extensibility in the articles made from a thermoplastic vulcanizate.

Description

FIELD OF INVENTION

- 5 [0001] Thermoplastic vulcanizates from thermoplastic polypropylene and a rubber can be modified with a random propylene copolymer polymerized with single site catalyst such as metallocene catalyst. This modification typically results in an improved elongation to break and toughness.

BACKGROUND OF THE INVENTION

- 10 [0002] Thermoplastic vulcanizates are comprised of a thermoplastic phase and a crosslinked rubbery phase and desirably have the thermoplastic processing properties of the thermoplastic phase and a substantial amount of elasticity from the rubber phase. The Shore A/D hardness of a thermoplastic vulcanizate is generally controlled by the ratio of the harder thermoplastic phase to the softer rubber phase. The elongation to break of a thermoplastic vulcanizate is controlled by many factors including compatibility of the two phases, phase sizes, and added compatibilizers. It is desirable to be able to formulate a thermoplastic vulcanizate composition to have higher elongation to break and more toughness. Toughness is defined as the area under the stress strain curve when a tensile specimen of the thermoplastic vulcanizate is elongated to break.

20 SUMMARY OF THE INVENTION

- [0003] Thermoplastic vulcanizates from a polypropylene thermoplastic phase and generally any rubber phase can be modified with random propylene copolymers polymerized with single site catalyst including metallocene catalyst to improve the physical properties of the thermoplastic vulcanizate. The random propylene copolymers can have from about 5 to about 25 weight percent of other ethylenically unsaturated monomers and more desirably from about 6 to about 20 weight percent of other ethylenically unsaturated monomers. Preferred ethylenically unsaturated monomers are ethylene or a monoolefin having from 4 to 20 carbon atoms. The residual of the random propylene copolymers is desirably repeat units derived from the polymerization of propylene. Desirably the repeat units from propylene are predominantly in either an isotactic or a syndiotactic configuration. The random propylene copolymer with crystallizable repeat units derived from propylene has a melting point above 0°C. The relative amount of the random propylene copolymer to the polypropylene thermoplastic is desirably from about 2 to about 400 parts by weight of random propylene copolymer per 100 parts by weight polypropylene thermoplastic and more desirably from about 5 to about 150 parts of random copolymer per 100 parts polypropylene thermoplastic. The propylene thermoplastic is desirably an isotactic polypropylene with a high melting temperature but can be any polypropylene other than said random copolymer. For the purpose of this specification we will distinguish between polypropylene thermoplastics which have a melting temperature of at least 120°C and random propylene copolymer which have a melting temperature below 105. The rubbers can be traditional hydrocarbon rubbers such as EPDM rubber, butyl rubber, halobutyl rubber, copolymers of p-methylstyrene and isobutylene, natural rubber, homopolymers of conjugated dienes, and copolymers of conjugated dienes or combinations thereof. Thermoplastic vulcanizates usually comprise from about 15 to about 75 parts of the thermoplastic phase and from about 25 to about 85 parts of the rubber phase based upon 100 parts total of the thermoplastic and rubber phases.

DETAILED DESCRIPTION

- 45 [0004] The random propylene copolymers used to modify the thermoplastic vulcanizates of this disclosure are copolymers of propylene with statistical insertion at least one other comonomer, other than propylene, into the polymer. Comonomers comprise ethylene and alpha-olefins having 4 to 20 carbon atoms. The arrangement of the propylene units is substantially isotactic or syndiotactic. The random propylene copolymers have narrow molecular weight distributions with a polydispersity index of less than 4. They can conveniently be prepared with single site catalyst, including metallocene catalysts, although the disclosure is not limited to those catalysts but rather to a random propylene copolymer and the thermoplastic vulcanizate composition with a random propylene copolymer. Metallocene catalyst are further described in U.S. Patent 5,017,714 herein incorporated by reference for its teachings on making random propylene copolymers. The random propylene copolymers have a low level of crystallinity with a heat of fusion of less than 65 or 75 J/g.
- 55 [0005] Prior to the development of metallocene catalyst it was very difficult to prepare random propylene copolymers having narrow molecular weight distribution with a polydispersity index of less than 4 or 5 with more than about 3 or 6 weight percent of a second comonomer. Rubbery copolymers such as EPDM or EPR rubber were available. Now it is possible to prepare thermoplastic random copolymers with from about 2 to about 16 or 20 weight percent of a second

comonomer or comonomers. Prior art pseudorandom propylene copolymer was made by a polymerization with a propylene feed and a second olefin feed, said second olefin generally having 2 or 4 to 8 or 12 carbon atoms, keeping a relatively constant feed ratio. The catalysts used would have several different active sites such that some sites incorporate the second olefin more efficiently than others. The different sites also can result in different polymer chain lengths.

This results in a broad molecular weight distribution and a broad compositional distribution of propylene in the resulting polymer.

[0006] The random propylene copolymer of this invention desirably have a narrow compositional distribution. While not meant to be limited thereby, it is believed that the narrow composition distribution of the random propylene copolymer is important. We believe that the narrow compositional distribution is a result of using a single sited catalyst (such as metallocene) which allows only a single statistical mode of addition of ethylene and propylene. We believe this results in no statistically significant difference in the composition of the polymer among two polymer chains. The intermolecular composition distribution of the polymer is determined by thermal fractionation in a solvent. A typical solvent is a saturated hydrocarbon such as hexane or heptane. This thermal fractionation procedure is described below. Typically, approximately 75 percent by weight and more preferably 85 percent by weight of the polymer is isolated as a one or two adjacent, soluble fraction with the balance of the polymer in immediately preceding or succeeding fractions. Each of these fractions has a composition (weight percent ethylene content) with a difference of no greater than 20 weight percent (relative) of the average weight percent ethylene content of the random propylene copolymer component. The random propylene copolymer is narrow in compositional distribution if it meets the fractionation test outlined above.

[0007] In the random propylene copolymer the number and distribution of ethylene residues is consistent with the statistical polymerization of ethylene, propylene and optional amounts of diene. In stereoblock structures, the number of monomer residues of any one kind adjacent to one another is greater than predicted from a statistical distribution in random propylene copolymers with a similar composition. Historical polymers with stereoblock structure have a distribution of ethylene residues consistent with these blocky structures rather than a statistical distribution of the monomer residues in the polymer. The intramolecular composition distribution of the polymer may be determined by C-13 NMR which locates the ethylene residues in relation to the neighboring propylene residue. A statistical distribution of the ethylene and propylene sequences will result for a polymer if (1) it is made with a single sited catalyst, such as a single site metallocene catalyst, which allows only a single statistical mode of addition of ethylene and propylene and (2) it is made in a well mixed, continuous monomer feed stirred tank polymerization reactor which allows only a single polymerization mode for substantially all of the polymer chains and (3) the catalyst has a product of reactivity ratios for ethylene and propylene less than 1.2. These polymerization parameters are needed for the formation of a random propylene copolymer.

[0008] The random propylene copolymer preferably has a single melting point. The melting point is determined by DSC. Generally, the random propylene copolymer has a melting point between about 0, 25 or 30°C and 105°C. Preferably, the melting point is between about 0, 25 or 30, or 40° and 90 or 100°C. Most preferably, the melting point is between 40°C and 90°C. For the purpose of this application a melting point will be the peak in the DSC determination of melting point. The random propylene copolymer preferably has a narrow molecular weight distribution (MWD) between about 1.5, 1.7 or 1.8 to about 3.5, 4.0 or 5.0, with a MWD between about 1.5, 1.8 or 2.0 to about 2.8 or 3.2 preferred.

[0009] The random propylene copolymer desirably comprises isotactically crystallizable alpha-olefin sequences, e.g., preferably propylene sequences (NMR). The crystallinity is, preferably, from about 2 to about 65 percent of homoisotactic polypropylene, preferably between 5 to 40 percent, as measured by the heat of fusion of annealed samples of the polymer.

[0010] The random propylene copolymer desirably comprises from about 75 or 80 to 95 percent by weight repeat units from propylene and from about 5 to about 20 or 25 percent by weight of repeat units from a linear or branched olefin other than propylene having 2 or from 4 to 8, 12, or 20 carbon atoms, preferably from about 80 to about 94 percent by weight repeat units from propylene and from about 6 to about 20 percent by weight of an alpha-olefin and most preferably, from about 80 or 82 to about 90 or 94 percent by weight repeat units from propylene and from about 6 or 10 to about 18 or 20 percent by weight and even more preferably between 10 to 16 percent by weight of said alpha-olefin and from about 84 to 90 percent by weight of propylene. Preferably said alpha-olefin is ethylene.

[0011] Notwithstanding, the recitation of a random propylene copolymer, it may be advantageous to add a mixture of two (preferred) or two or more random propylene copolymers. Each of the random propylene copolymers in the mixture of random propylene copolymers desirably satisfies the description of the individual random propylene copolymer. The random propylene copolymers can differ in their weight or number average molecular weight and more preferably differ in composition by having different amounts of comonomer incorporated in the copolymerization with propylene and different amounts of crystallinity. It is particularly advantageous to have a first random propylene copolymer having a melting point above 70°C and with greater than 93 percent weight repeat units from propylene while the second random propylene copolymer has a melting point below 60°C with less than 92 percent weight repeat units from propylene. Alternatively it is desirable that the first random propylene copolymer has between about 20 or 25 and about 65% of the

crystallinity of a homoisotactic polypropylene, as measured by the heat of fusion of annealed samples. The second random propylene copolymer would desirably have less crystallinity than the first. It is believed that the first random propylene copolymer when used in conjunction with the second and a thermoplastic polypropylene, acts as an interfacial agent. Thus the first random copolymer can result in a morphology with a finer dispersion of a dispersed phase and any resultant properties from the finer (smaller particle size) dispersion. The ratio of the first and the second random propylene copolymer in this mixture may range from 95:5 to 5:95 with preference for ratios in the range 90:10 to 10:90.

[0012] We believe that the addition of random propylene copolymers which consist of two and less preferably more than two individual random propylene copolymers as described above will lead to improvements in the production and in the properties of the thermoplastic vulcanizate. The improvements in the production will include the ability to introduce pellets of a substantially amorphous random propylene copolymer (rubber) while the improvements in the properties will include improvements in the tensile strength, elongation at break, and low temperature impact strength beyond that which has been demonstrated by the addition of a single random propylene copolymer.

[0013] There is no particular limitation on the method for preparing the random propylene copolymer component of the invention. Random propylene copolymers may be obtained by copolymerizing propylene and an alpha-olefin having 2 or from 4 to about 20 carbon atoms, preferably ethylene, in a single stage or multiple stage reactor. Polymerization methods include high pressure, slurry, gas, bulk, or solution phase, or a combination thereof, using a traditional Ziegler-Natta catalyst or a single-site, metallocene catalyst system. The catalyst used is preferably one which has a high isospecificity. Polymerization may be carried out by a continuous or batch process and may include use of chain transfer agents, scavengers, or other such additives as deemed applicable.

[0014] Generally, without limiting in any way the scope of the invention, one embodiment for carrying out the production of the random propylene copolymer is as follows: (1) liquid propylene is introduced in a stirred-tank reactor, (2) the catalyst system is introduced via nozzles in either the vapor or liquid phase, (3) feed ethylene gas is introduced either into the vapor phase of the reaction, or sparged into the liquid phase, as is well known in the art, (4) the reactor contains a liquid phase composed substantially of propylene, together with dissolved alpha-olefin, preferably ethylene, and a vapor phase containing vapors of all monomers, (5) the reactor temperature and pressure may be controlled via reflux of vaporizing propylene (autorefrigeration), as well as by cooling coils, jackets, etc., (6) the polymerization rate is controlled by the concentration of catalyst, temperature, and (7) the ethylene (or other alpha-olefin) content of the polymer product is determined by the ratio of ethylene to propylene in the reactor, which is controlled by manipulating the relative feed rates of these components to the reactor.

[0015] For example, a typical polymerization process for the random propylene copolymer consists of a polymerization in the presence of a catalysts comprising a bis (cyclopentadienyl) metal compound and either 1) a non-coordinating compatible anion activator, or 2) an alumoxane activator. This comprises the steps of contacting ethylene and propylene with a catalyst in a suitable polymerization diluent, said catalyst comprising, for example, according to a preferred embodiment, a chiral metallocene catalyst, e.g., a bis (cyclopentadienyl) metal compound, as described in U.S. Patent No. 5,198,401 which is herein incorporated by reference for purposes of U.S. practices, and an activator. The activator used may be an alumoxane activator or a non-coordination compatible anion activator.

[0016] The alumoxane activator is preferably utilized in an amount to provide a molar aluminum to metallocene ratio of from about 1:1 to about 20,000:1 or more. The non-coordinating compatible anion activator is preferably utilized in an amount to provide a molar ratio of biscyclopentadienyl metal compound to non-coordinating anion of 10:1 to about 1:1. The above polymerization reaction is conducted by reacting such monomers in the presence of such catalyst system at a temperature of from about -100°C to about 300°C for a time of from about 1 second to about 10 hours to produce a copolymer having a weight average molecular weight of from about 5,000 or less to about 1,000,000 or more and a molecular weight distribution of from about 1.8 to about 4.5.

[0017] While the process in some embodiments includes utilizing a catalyst system in the liquid phase (slurry, solution, suspension or bulk phase or combination thereof), according to other embodiments, high pressure fluid phase or gas phase polymerization can also be utilized. When utilized in a gas phase, slurry phase or suspension phase polymerization, the catalyst systems will preferably be supported catalyst systems. See, for example, U.S. Patent No. 5,057,475 which is incorporated herein by reference for purposes of U.S. practice. Such catalyst systems can also include other well known additives such as, for example, scavengers. See, for example, U.S. Patent No. 5,153,157 which is incorporated herein by reference for purposes of U.S. practices. These processes may be employed without limitation of the type of reaction vessels and the mode of conducting the polymerization. As stated above, and while it is also true for systems utilizing a supported catalyst system, the liquid phase process comprises the steps of contacting ethylene and propylene with the catalyst system in a suitable polymerization diluent and reacting the monomers in the presence of the catalyst system for a time and at a temperature sufficient to produce an ethylene-propylene copolymer of the desired molecular weight and composition.

[0018] The random propylene copolymer can be 1) incorporated into the components used to form a thermoplastic vulcanizate (TPV), 2) blended with a TPV composition prior to vulcanization of the rubber component, or 3) added after said vulcanization of said TPV. The physical properties of the resulting blend may or may not vary depending upon

whether the random propylene copolymer was added prior to or subsequent to vulcanization of the rubber phase. The random propylene copolymer can be considered a supplement to the semi-crystalline polypropylene of the thermoplastic vulcanizate or can be considered to be substituted on a weight basis for the semi-crystalline polypropylene in a thermoplastic vulcanizate. When the random propylene copolymer is added prior to vulcanization, it is anticipated that a majority of the random propylene copolymer is in the thermoplastic phase of the resulting thermoplastic vulcanizate, although it may be disproportionately present at the interface between the rubber phase and the thermoplastic phase. Since the secant modulus of the random propylene copolymer is lower than that of the semi-crystalline polypropylene, it is readily melt-blendable with the thermoplastic vulcanizate or the components thereof at the normal processing/mixing temperatures for the thermoplastic vulcanizate.

[0019] The major portion of polymers in the thermoplastic vulcanizate are the conventional polypropylene thermoplastic; the random propylene copolymer, and a crosslinkable rubber. Examples of conventional semi-crystalline polypropylene are polypropylene, its copolymers and mixtures thereof

[0020] The total of the conventional semi-crystalline polypropylene and the random propylene copolymer is desirably from about 6 to about 85 weight percent, more desirably from about 7 to about 75, and preferably from about 8 to about 60 weight percent when based upon the total of the compounded thermoplastic vulcanizate. Desirably the rubber is from about 5 to about 70, more desirably about 10 to about 50 and preferably from about 15 to 45 weight percent of the thermoplastic vulcanizate. Desirably the other conventional components to TPV, e.g. fillers, oils, curatives, processing aids, etc., are from about 0, 1, 2, or 10 to about 87, 88 or 89 weight percent of the TPV, more desirably from about 0, 1, 2, or 15 to about 81, 82 or 83 and preferably from about 0, 1, 2, or 25 to about 75, 76 or 79 weight percent.

[0021] Minor amounts of other polymers may be added to modify flow properties, or as additives, such as polymeric antioxidants. Non-polymeric materials such as oils, fillers, diluents and additives (discussed in a later paragraph) may be present in large amounts. Amounts of most of the components to the blend will be specified either 1) per 100 parts by weight of the blend of the conventional semi-crystalline polypropylene, random propylene copolymer, and the rubber or 2) per 100 parts by weight of rubber.

[0022] The total of the semi-crystalline polypropylene and the random propylene copolymer is desirably from about 15 to about 80 parts by weight, more desirably from about 25 to about 75 parts by weight, and preferably from about 25 to about 50 parts by weight per 100 parts of the blend of semi-crystalline polypropylene, random propylene copolymer, and the rubber. The rubber is desirably from about 20 to about 85 parts by weight, more desirably from about 25 to about 75 parts by weight and preferably from about 50 to about 75 parts by weight per 100 parts by weight of said blend. If the amount of semi-crystalline polypropylene is based on the amount of rubber, it is desirably from about 17.5 to about 320 parts by weight, more desirably from about 33 to about 300 parts and preferably from about 33 to about 200 parts by weight per 100 parts by weight of the rubber.

[0023] The random propylene copolymer is desirably present in amounts from about 2 to about 400 parts per 100 parts of conventional polypropylene in the thermoplastic vulcanizate, more desirably in amounts from about 5 to about 150 parts per 100 parts of polypropylene, still more desirably from about 10 or 25 to about 100 parts per 100 parts by weight of conventional polypropylene, and preferably from about 25 to about 80 parts by weight per 100 parts by weight of conventional polypropylene. Thus the random propylene copolymer may be present in amounts from about 4 to about 80 and more desirably about 4 or 20 to about 60 weight percent of the thermoplastic phase of the thermoplastic vulcanizate. Since the thermoplastic phase of the thermoplastic vulcanizate can be from about 15 to about 75 percent of the blend of the thermoplastic and rubber phase (without fillers, oils, etc.), the percentage of random propylene copolymer based upon the total weight of the thermoplastic vulcanizate can range from 1 or 2 to about 40, 50 or 60 weight percent based upon either the combined weight of the conventional polypropylene, random propylene copolymer and rubber components (without fillers, oils etc.).

[0024] The terms "blend" and "thermoplastic vulcanizate" used herein mean a mixture ranging from small particles of crosslinked rubber well dispersed in a semi-crystalline polypropylene matrix to co-continuous phases of the semi-crystalline polypropylene and a partially to fully crosslinked rubber or combinations thereof. The term "thermoplastic vulcanizate" indicates the rubber phase is at least partially vulcanized (crosslinked).

[0025] The term "thermoplastic vulcanizate" refers to compositions that may possess the properties of a thermoset elastomer and are reprocessible in an internal mixer. Upon reaching temperatures above the softening point or melting point of the semi-crystalline polypropylene phase, they can form continuous sheets and/or molded articles with what visually appears to be complete knitting or fusion of the thermoplastic vulcanizate under conventional molding or shaping conditions for thermoplastics.

[0026] Subsequent to dynamic vulcanization (curing) of the rubber phase of the thermoplastic vulcanizate, desirably less than 20 or 50 weight percent of the curable rubber is extractable from the specimen of the thermoplastic vulcanizate in boiling xylene. Techniques for determining extractable rubber as set forth in U.S. Patent 4,311,628, are herein incorporated by reference.

[0027] The conventional semi-crystalline polypropylene comprises semi-crystalline thermoplastic polymers from the polymerization of monoolefin monomers (e.g. 2 to 10 carbon atoms) by a high pressure, low pressure, or intermediate

pressure process: or by Ziegler-Natta catalysts, or by metallocene catalysts. It may have any tacticity (e.g. isotactic and syndiotactic) or be a copolymer such as impact modified polypropylene. Desirably the monoolefin monomers converted to repeat units are at least 80, 85 or 93 percent propylene. The polypropylene can be a homopolymer, a reactor copolymer polypropylene impact modified propylene, isotactic polypropylene, syndiotactic polypropylene, impact copolymer polypropylene and other prior art propylene copolymers. Desirably it has a melting temperature peak of at least 120°C and a heat of fusion of greater than 75, 80, or 90 J/g.

[0028] The rubber can be a rubber that can react and be crosslinked under crosslinking conditions. These rubbers can include natural rubber, EPDM rubber, butyl rubber, halobutyl rubber, halogenated (e.g. brominated) copolymers of p-alkylstyrene and an isomonoolefin having from 4 to 7 carbon atoms (e.g. isobutylene), butyl rubbers containing repeat units from divinyl benzene, homo or copolymers from at least one conjugated diene, or combinations thereof. EPDM, butyl and halobutyl rubbers are referred to as rubbers low in residual unsaturation and are preferred when the vulcanizate needs good thermal stability or oxidative stability. The rubbers low in residual unsaturation desirably have less than 10 weight percent repeat units having unsaturation. Desirably excluded from rubbers are acrylate rubber and epichlorohydrin rubber. For the purpose of this invention, copolymers will be used to define polymers from two or more monomers, and polymers can have repeat units from one or more different monomers.

[0029] The rubber is desirably an olefin rubber such as EPDM-type rubber. EPDM-type rubbers are generally terpolymers derived from the polymerization of at least two different monoolefin monomers having from 2 to 10 carbon atoms, preferably 2 to 4 carbon atoms, and at least one polyunsaturated olefin having from 5 to 20 carbon atoms. Said monoolefins desirably have the formula $\text{CH}_2=\text{CH}-\text{R}$ where R is H or an alkyl of 1-12 carbon atoms and are preferably ethylene and propylene. Desirably the repeat units from at least two monoolefins (and preferably from ethylene and propylene) are present in the polymer in weight ratios of 25:75 to 75:25 (ethylene:propylene) and constitute from about 90 to about 99.6 weight percent of the polymer. The polyunsaturated olefin can be a straight chained, branched, cyclic, bridged ring, bicyclic, fused ring bicyclic compound, etc., and preferably is a nonconjugated diene. Desirably repeat units from the nonconjugated polyunsaturated olefin is from about 0.4 to about 10 weight percent of the rubber.

[0030] The rubber can be a butyl rubber, halobutyl rubber, or a halogenated (e.g. brominated) copolymer of p-alkylstyrene and an isomonoolefin of 4 to 7 carbon atoms. "Butyl rubber" is defined a polymer predominantly comprised of repeat units from isobutylene but including a few repeat units of a monomer which provides sites for crosslinking. The monomers which provide sites for crosslinking can be a polyunsaturated monomer such as a conjugated diene or divinyl benzene. Desirably from about 90 to about 99.5 weight percent of the butyl rubber are repeat units derived from the polymerization of isobutylene, and from about 0.5 to about 10 weight percent of the repeat units are from at least one polyunsaturated monomer having from 4 to 12 carbon atoms. Preferably the polyunsaturated monomer is isoprene or divinylbenzene. The polymer may be halogenated to further enhance reactivity in crosslinking. Preferably the halogen is present in amounts from about 0.1 to about 10 weight percent, more preferably about 0.5 to about 3.0 weight percent based upon the weight of the halogenated polymer; preferably the halogen is chlorine or bromine. The brominated copolymer of p-alkylstyrene, having from about 9 to 12 carbon atoms, and an isomonoolefin, having from 4 to 7 carbon atoms, desirably has from about 88 to about 99 weight percent isomonoolefin, more desirably from about 92 to about 98 weight percent, and from about 1 to about 12 weight percent p-alkylstyrene, more desirably from about 2 to about 8 weight percent based upon the weight of the copolymer before halogenation. Desirably the alkylstyrene is p-methylstyrene and the isomonoolefin is isobutylene. Desirably the percent bromine is from about 0.2 to about 8, more desirably from about 0.2 to about 3 weight percent based on the weight of the halogenated copolymer. The copolymer is a complementary amount, i.e., from about 92 to about 99.8, more desirably from about 97 to about 99.8 weight percent. These polymers are commercially available from Exxon Chemical Co.

[0031] Other rubber such as natural rubber or synthetic homo or copolymers from at least one conjugated diene can be used in the dynamic vulcanizate. These rubbers are higher in unsaturation than EPDM rubber and butyl rubber. The natural rubber and said homo or copolymers of a diene can optionally be partially hydrogenated to increase thermal and oxidative stability. The synthetic rubber can be nonpolar or polar depending on the comonomers. Desirably the homo or copolymers of a diene have at least 50 weight percent repeat units from at least one conjugated diene monomer having from 4 to 8 carbon atoms. Comonomers may be used and include vinyl aromatic monomer(s) having from 8 to 12 carbon atoms and acrylonitrile or alkyl-substituted acrylonitrile monomer(s) having from 3 to 8 carbon atoms. Other comonomers desirably used include repeat units from monomers having unsaturated carboxylic acids, unsaturated dicarboxylic acids, unsaturated anhydrides of dicarboxylic acids, and include divinylbenzene, alkylacrylates and other monomers having from 3 to 20 carbon atoms. Examples of synthetic rubbers include synthetic polyisoprene, polybutadiene rubber, styrene-butadiene rubber, butadiene-acrylonitrile rubber, etc. Amine-functionalized, carboxy-functionalized or epoxy-functionalized synthetic rubbers may be used, and examples of these include maleated EPDM, and epoxy-functionalized natural rubbers. These materials are commercially available.

[0032] The thermoplastic vulcanizates of this disclosure are generally prepared by melt-mixing in any order, the semi-crystalline polyolefin(s) (e.g. polypropylene thermoplastic), the random propylene copolymer, the rubber, and other ingredients (filler, plasticizer, lubricant, stabilizer, etc.) in a mixer heated to above the melting temperature of the poly-

propylene thermoplastic. The optional fillers, plasticizers, additives etc., can be added at this stage or later. After sufficient molten-state mixing to form a well mixed blend, vulcanizing agents (also known as curatives or crosslinkers) are generally added. In some embodiments it is preferred to add the vulcanizing agent in solution with a liquid, for example rubber processing oil, or in a masterbatch which is compatible with the other components. It is convenient to follow the progress of vulcanization by monitoring mixing torque or mixing energy requirements during mixing. The mixing torque or mixing energy curve generally goes through a maximum after which mixing can be continued somewhat longer to improve the fabricability of the blend. If desired, one can add some of the ingredients after the dynamic vulcanization is complete. The random polypropylene copolymer can be added before, during, or after vulcanization. After discharge from the mixer, the blend containing vulcanized rubber and the thermoplastic can be milled, chopped, extruded, pelletized, injection-molded, or processed by any other desirable technique. It is usually desirable to allow the fillers and a portion of any plasticizer to distribute themselves in the rubber or semi-crystalline polypropylene phase before the rubber phase or phases are crosslinked. Crosslinking (vulcanization) of the rubber can occur in a few minutes or less depending on the mix temperature, shear rate, and activators present for the curative. Suitable curing temperatures include from about 120°C or 150°C to about 250°C, more preferred temperatures are from about 150°C or 170°C to about 225°C or 250°C. The mixing equipment can include Banbury™ mixers, Brabender™ mixers, multiroll mills and certain mixing extruders.

[0033] The thermoplastic vulcanizate can include a variety of additives. The additives include particulate fillers such as carbon black, silica, titanium dioxide, colored pigments, clay; zinc oxide; stearic acid; stabilizers; anti-degradants; flame retardants; processing aids; adhesives; tackifiers; plasticizers; wax; discontinuous fibers (such as wood cellulose fibers) and extender oils. When extender oil is used it can be present in amounts from about 5 to about 300 parts by weight per 100 parts by weight of the blend of semi-crystalline polypropylene and rubber. The amount of extender oil (e.g., hydrocarbon oils and ester plasticizers) may also be expressed as from about 30 to 250 parts, and more desirably from about 70 to 200 parts by weight per 100 parts by weight of said rubber. When non-black fillers are used, it is desirable to include a coupling agent to compatibilize the interface between the non-black fillers and polymers. Desirable amounts of carbon black, when present, are from about 5 to about 250 parts by weight per 100 parts by weight of rubber.

[0034] Another component to the dynamic vulcanizate is the curative which crosslinks or vulcanizes the crosslinkable rubber phase. The type of curative used in this disclosure depends on the type of rubber to be crosslinked. The curatives for each type of rubber are conventional for those rubbers in thermoplastic vulcanizates and are used in conventional amounts. The curatives include, but are not limited to, phenolic resin curatives, sulfur curatives, with or without accelerators, accelerators alone, peroxide curatives, hydrosilation curatives using silicon hydride and platinum or peroxide catalyst, etc.

[0035] Thermoplastic vulcanizate compositions of the invention are useful for making a variety of articles such as tires, hoses, belts, gaskets, moldings and molded parts. They are particularly useful for making articles by extrusion, injection molding, blow molding, and compression molding techniques. They also are useful for modifying thermoplastic resins and in particular polyolefin resins. The compositions can be blended with thermoplastic resins using conventional mixing equipment making a rubber modified thermoplastic resin. The properties of the modified thermoplastic resin depend upon the amount of thermoplastic vulcanizate composition blended.

[0036] The stress-strain properties of the compositions are determined in accordance with the test procedures set forth in ASTM D412. These properties include tension set (TS), ultimate tensile strength (UTS), 50 percent modulus (M50), 100 percent modulus (M100), and ultimate elongation at break (UE). The tear strength is measured according to ASTM D623. The hardness is measured according to ASTM D2240, with a 5 second delay using either the Shore A or Shore D scale. Compression set (CS) is determined in accordance with ASTM D-395, Method B, by compressing the sample for 22 hours at 100°C. Oil swell (OS) (percent change in weight) is determined in accordance with ASTM D-471 by submerging the specimen in IRM 903 oil and unless otherwise specified is for 24 hours at 125±2°C. Especially preferred compositions of the invention are rubbery compositions having tension set values of about 50 percent or less which compositions meet the definition for rubber as defined by ASTM Standards, V. 28, page 756 (D1566). More preferred compositions are rubbery compositions having a Shore D hardness of 60 or below, or a 100 percent modulus of 18 MPa or less, or a Young's modulus below 250 MPa.

EXAMPLES

[0037] The composition of ethylene propylene copolymers, which are used as comparative examples of Tables I-III, was measured as ethylene weight percent according to ASTM D 3900. The composition of the random propylene copolymer of Tables I-III was measured as ethylene weight percent according to the following technique. A thin homogeneous film of the copolymer, pressed at a temperature of about or greater than 150°C was mounted on a Perkin Elmer PE 1760 infra red spectrophotometer. A full spectrum of the sample from 600 cm⁻¹ to 400 cm⁻¹ was recorded and the ethylene weight percent of the polymer was calculated according to Equation 1 as follows:

$$\text{ethylene wt. \%} = 82.585 - 111.987X + 30.045X^2$$

(Equation 1)

wherein X is the ratio of the peak height at 1155 cm^{-1} and peak height at either 722 cm^{-1} or 732 cm^{-1} , which ever is higher.

[0038] Techniques for determining the molecular weight (Mn and Mw) and molecular weight distribution (MWD) are found in U.S. Patent 4,540,753 (Cozewith, Ju and Verstrate) (which is incorporated by reference herein for purposes of U.S. practices) and references cited therein and in *Macromolecules*, 1988, volume 21, p 3360 (Verstrate et al) (which is herein incorporated by reference for purposes of U.S. practice) and references cited therein.

[0039] The procedure for Differential Scanning Calorimetry of Tables I-III follows. About 6 to 10 mg of a sheet of the polymer pressed at approximately 200°C to 230°C is removed with a punch die. This is annealed at room temperature for 80 to 100 hours. At the end of this period, the sample is placed in a Differential Scanning Calorimeter (Perkin Elmer 7 Series Thermal Analysis System) and cooled to about -50°C to about -70°C . The sample is heated at $20^{\circ}\text{C}/\text{min}$ to attain a final temperature of about 200°C to about 220°C . The thermal output is recorded as the area under the melting peak of the sample, which is typically peaked at about 30°C to about 175°C and occurs between the temperatures of about 0°C and about 200°C , and is measured in Joules as a measure of the heat of fusion. The melting point is recorded as the temperature of the greatest heat absorption within the range of melting of the sample. Under these conditions, the melting point of the random propylene copolymer and the heat of fusion is lower than for a polypropylene homopolymer.

[0040] Composition distribution of the random propylene copolymer was measured as described below. About 30 gms. of the random propylene copolymer was cut into small cubes about $1/8''$ on the side. This is introduced into the thick walled glass bottle closed with screw cap along with 50 mg of Irganox 1076, an antioxidant commercially available from Ciba-Geigy Corporation. Then, 425 ml of hexane (a principal mixture of normal and iso isomers) is added to the contents of the bottle and the sealed bottle is maintained at about 23°C for 24 hours. At the end of this period, the solution is decanted and the residue is treated with additional hexane for an additional 24 hours. At the end of this period, the two hexane solutions are combined and evaporated to yield a residue of the polymer soluble at 23°C . To the residue is added sufficient hexane to bring the volume to 425 ml and the bottle is maintained at about 31°C for 24 hours in a covered circulating water bath. The soluble polymer is decanted and the additional amount of hexane is added for another 24 hours at about 31°C prior to decanting. In this manner, fractions of the polymer soluble at 40°C , 48°C , 55°C and 62°C are obtained at temperature increases of approximately 8°C between stages. Further, increases in temperature to 95°C can be accommodated, if heptane, instead of hexane, is used as the solvent for all temperatures above about 60°C . The soluble polymers are dried, weighed and analyzed for composition, weight percent ethylene content, by the IR technique described above. Soluble fractions obtained in the adjacent temperature increases are the adjacent fractions in the specification above.

[0041] SPC-1 through SPC-5 were prepared in a manner described in the specification for polymerizing a random propylene copolymer. Table I describes the results of the GPC, composition, ML and DSC analysis for the polymers and for some comparative polymers. EPR is Vistalon™ 457 an ethylene-propylene copolymer commercially available from EXXON Chemical Co., and ae PP is an experimental propylene copolymer containing 11.7 weight percent ethylene but no isotactic propylene sequences (i.e., it is totally amorphous). Experimental random propylene copolymers M-PP A through M-PP E and M-PP H are also characterized along with some conventional propylene copolymers and homopolymers. Table II describes the temperature and percent of each copolymer soluble in hexane at a certain temperature.

Table I

SPC	(Mn) by GPC	(Mw) by GPC	Ethylene wt% by wt% by IR	Heat of fusion J/g	Melting Point by DSC (°C)	ML (1+4)- @125°C
SPC-1	102000	248900	7.3	71.9	84.7	14
SPC-2	124700	265900	11.6	17.1	43.0	23.9
SPC-3	121900	318900	16.4	7.8	42.2	33.1
SPC-4			11.1	25.73	63.4	34.5
SPC-5			14.7	13.2	47.8	38.4
Expt M-PP A			13.1	12.4	52.1	16.4
Expt M-PP B	N/A	N/A	12.1	22.5	54.1	11.6
Expt M-PP C	N/A	N/A	14.9	14.6	52.1	6.4
Expt M-PP D	N/A	N/A	9	40.5	81.8	34.7
Expt M-PP E	N/A	NA	7.5	41.8	90.2	8.8
Expt M-PP H	N/A	N/A	7.3	35.6	85.1	14
Comparative Polymers						
EPR	-	-	46.8	not detected	not detected	-
aePP	-	-	11.7	not detected	not detected	-
Reflex			0	23.9	154°C	
D100						
Reflex D1700			0	62.2	158°C	
Reflex D2300			0		156°C	
Reflex D2330			0		-	
Impact Escorene PD 7302			0.5	84.1	163	
Lyondell 51S07A			0	92.9	164.7	

Table II

Solubility of the Propylene Copolymers				
SPC	Wt. % soluble at 23°C	Wt. % soluble at 31°C	Wt. % soluble at 40°C	Wt. % soluble at 48°C
SPC-1	1.0	2.9	28.3	68.5
SPC-2	6.5	95.7	-	-
SPC-3	51.6	52.3	2.6	-
SPC-4	18.7	83.6	-	-
SPC-5	36.5	64.2	-	-
Comparative Polymers				
EPR	101.7	-	-	-
aePP	100.5	-	-	-

Sum of the fractions add up to slightly more than 100 due to imperfect drying of the polymer fractions.

[0042] Table III describes the composition of the fractions of the propylene copolymers obtained in Table II. Only fractions which have more than 4% of the total mass of the polymer have been analyzed for composition.

[0043] Table IV characterizes the compositions of thermoplastic vulcanizates (TPVs) used in later tables. The TPVs also comprise crosslinks from a crosslinking agent, and preferably fillers, oils, process aids, etc.

[0044] Table V compares an unmodified TPV from polypropylene and EPDM to the same TPV modified with 1) a polypropylene homopolymer (Lyondell 51S70A), 2) four different random propylene copolymers (A-D), and 3) a conventional propylene copolymer.

Table III

Weight Percent Ethylene in Fraction					
SPC	soluble at 23°C	soluble at 31°C	soluble at 40°C	soluble at 48°C	soluble at 56°C
SPC-1	-	-	8.0	7.6	-
SPC-2	12.0	11.2	-	-	-
SPC-3	16.8	16.5	-	-	-
SPC-4	13.2	11.2	-	-	-
SPC-5	14.9	14.6	-	-	-
Comparative Polymers					
EPR	46.8				
atactic ePP	11.8				

The experimental inaccuracy in determination of the ethylene content is believed to about 0.4 wt. % absolute.

Table IV

Thermoplastic Vulcanizates: Rubber Type, Polypropylene Concentration and Rubber Concentration			
Thermoplastic Vulcanizate	Rubber Type	PP Concentration, wt. %	Rubber Concentration wt. %
TPV-1	EPDM	13.4%	28.5%
TPV-2	EPDM	58.3%	14.5%

EP 0 969 043 A1

Table IV (continued)

Thermoplastic Vulcanizates: Rubber Type, Polypropylene Concentration and Rubber Concentration			
Thermoplastic Vulcanizate	Rubber Type	PP Concentration, wt. %	Rubber Concentration wt. %
TPV-3	EPDM	9.4%	26.7%
TPV-4	Nitrile	15.0%	48.0%
TPV-5	Butyl	16.0%	42.0%

Table V

Blends of an EPDM/Polypropylene TPV with Polypropylene or Metallocene Catalyzed Propylene Copolymers or Conventional Polypropylene Copolymer								
	1C	2C	3C	4	5	6	7	8C
TPV-1	100	100	100	100	100	100	100	100
Lyondell 51S07A		6.7	13.4					
Expt M-PP A				13.4				
Expt M-PP B					13.4			
Expt M-PP C						13.4		
Expt M-PP D							13.4	
Escorene PD9272								13.4
Final Brabender Torque	-	-	650	540	500	510	575	480
PP Copolymer Concentration, wt.	0.0%	0.0%	0.0%	11.8%	11.8%	11.8%	11.8%	11.8%
PP:PP Copolymer ratio								
Hardness, Shore A	61	70	83	61	63	60	70	77
50% Modulus, MPa	1.73	2.67	3.65	1.66	1.83	1.54	2.46	3.12
100 % Modulus, MPa	2.45	3.46	4.46	2.25	2.45	2.10	3.16	3.88
Tensile Strength, MPa	5.73	6.95	8.68	6.45	6.63	5.22	10.05	8.39
Ultimate Elongation, %	401	439	433	530	514	492	585	471
Toughness, MJ/m ³	14.0	21.0	25.2	19.7	19.8	16.0	31.4	25.3
Tension Set, 100 % elongation, 10 minutes, room temperature								
% Set	7.5%	11.5%	16.0%	8.5%	9.5%	9.0%	11.5%	14.5%
Oil Swell, 24 hours, 125°C								
% wt gain	91.2	81.6	71	148.4	146.8	143	118.1	131.4
Compression Set 22, hours								
% Set @ 100°C	23	31	39	47	40	43	37	41

Table VI
Effect of Random Propylene Copolymer Composition on Properties of TPV Blend

	9C	10C	11C	12C	13	14	15	16
TPV-I	100	100	100	100	100	100	100	100
Expt M-PP C					3.35	6.7	10	13.4
Expt M-PP D								
Expt M-PP E								
PP:PP Copolymer Ratio	100:0	100:0	100:0	100:0	100:25	100:50	100:75	100:100
Final Brabender Torque	380	360	390	390	360	360	360	360
Physical Properties, Unaged								
Hardness, Shore A	62	62	62	62	61	59	58	58
50 % Modulus, MPa	1.70	1.73	1.72	1.72	1.63	1.59	1.53	1.51
100 % Modulus, MPa	2.39	2.41	2.40	2.41	2.30	2.22	2.12	2.07
Tensile Strength, MPa	5.43	5.83	5.78	5.19	5.38	5.16	5.05	5.49
Ultimate Elongation, %	407	443	438	397	433	454	480	542
Toughness, MJ/m ²	13.7	15.8	15.6	13.1	14.5	14.7	15.2	18.1
Tension Set, 100 % elongation, 10 minutes, room temperature								
% Set	7.5	9.0	7.5	8.0	7.0	8.0	9.0	8.5
Compression Set, 22 hours								
% Set @ 100C	24.1	26.4	25.6	27.3	29.9	33.1	39.8	46.2
Weight Gain								
% Swell @ 125C	97.4	98.3	97.4	96.4	115.1	131.2	134.6	140.2

Table VI
Effect of Random Propylene Copolymer Composition on Properties of TPV Blend

	17	18	19	20	21	22	23	24
TPV-1	100	100	100	100	100	100	100	100
Expt M-PP C								
Expt M-PP D	3.35	6.7	10.0	13.4				
Expt M-PP E					3.35	6.7	10.0	13.4
PP:PP Copolymer Ratio	100:25	100:50	100:75	100:100	100:25	100:50	100:75	100:100
Final Brabender Torque	400	400	430	440	380	380	370	370
Physical Properties, Unaged								
Hardness, Shore A	64	66	67	69	65	67	69	70
50 % Modulus, MPa	1.91	2.13	2.18	2.36	1.97	2.12	2.30	2.45
100 % Modulus, MPa	2.61	2.83	2.89	3.06	2.66	2.82	2.99	3.14
Tensile Strength, MPa	6.06	7.81	8.22	10.23	6.66	7.43	8.28	8.52
Ultimate Elongation, %	451	549	564	639	499	536	568	567
Toughness, MJ/m ³	16.9	24.8	26.4	34.2	20.06	23.5	27.0	27.9
Tension Set, 100 % elongation, 10 minutes, room temperature								
% Set	9.0	10.0	11.0	12.0	9.0	10.0	12.0	12.5
Compression Set, 22 hours								
% Set @ 100C	28.9	35.2	28.2	37.2	29.1	35.2	35.7	36.1
Weight Gain								
Oil Swell, 24 hours, 125°C	104.8	145.1	141.7	183.3	106.9	133.8	148.7	157.4

Table VI
Effect of Random Polypropylene Copolymer Composition
on Properties of TPV Blend

	25	26	27	28
TPV-1	100.0	100.0	100.0	100.0
Expt M-PP H	3.4	6.7	10.0	13.4
PP:PP Copolymer Ratio	100:25	100:50	100:75	100:100
Physical Properties, Unaged				
Hardness, Shore A	65	66	69	70
50 % Modulus, MPa	2.00	2.18	2.34	2.47
100 % Modulus, MPa	2.70	2.91	3.04	3.18
Tensile Strength, MPa	7.25	8.11	8.90	9.65
Ultimate Elongation, %	522	548	587	601
Toughness, MJ/m ³	22.13	25.46	29.07	31.69
Tension Set, 100 % elongation, 10 minutes, room temperature				
% Set	9.5	10.5	11.5	12.0

[0045] Table VI illustrates the properties of four different random propylene copolymers at different levels in a TPV.

[0046] Table VII shows the effect of adding a random propylene copolymer in four different amounts to a thermoplastic vulcanizates (TPV). The amounts of the random propylene copolymer are higher than shown in the previous tables. As can be seen from reading the table from left to right the experimental polypropylene copolymer increases the elongation to break, increases the toughness and increases the tear strength of the compositions. Due to the fact that the thermoplastic random propylene copolymer increases the relative ratio of the thermoplastic phase in these examples it generally increases the Shore A hardness and the modulus as the amount of random propylene copolymer increases.

[0047] Table VIII contains control examples that illustrate the effect of adding polypropylene homopolymers. While toughness increases, it is more a function of modulus increase than an increase in ultimate elongation.

[0048] Table IX illustrates the effect of adding traditional propylene copolymers to a TPV. Again as with propylene homopolymers, increases in toughness are due primarily to increases in modulus.

Table VII

Physical Properties of blends of TPV M-PP Copolymer where the M-PP copolymer concentration is greater than the PP homopolymer concentration					
	29C	30	31	32	33
Formulation, Phr					
TPV-1	100.0	100.0	100.0	100.0	100.0
Expt M-PP D		13.40	26.80	40.20	53.60
PP:PP Copolymer Ratio	100:0	100:100	100:200	100:300	100:400
Physical Properties, Unaged					
Hardness, Shore A	61	65	70	71	75
50 % Modulus, MPa	1.62	2.20	2.58	2.95	3.26
100 % Modulus, MPa	2.31	2.90	3.25	3.58	3.85
Tensile Strength, MPa	5.39	8.42	13.60	17.40	18.80
Ultimate Elongation, %	424	566	716	776	785
Toughness, MJ/m ³	14.07	26.86	45.73	58.58	63.82
Tension Set, % set	7.5	12.5	15	17	18

Table VIII

Effect of Low Density Polypropylene on TPV Blends							
	34C	35C	36C	37C	38C	39C	40C
TPV-1	100	100	100	100	100	100	100
Lyondell 51S70A ¹		13.4					
Reflex [®] D100			13.4				
Reflex [®] D1700				13.4			
Reflex [®] D2300						13.4	
Reflex [®] D2330							13.4
Physical Properties, Unaged							
Hardness, Shore A	63	81	65	75	63	70	68
50 % Modulus, MPa	1.72	3.47	2.00	2.72	1.72	2.21	2.12
100 % Modulus, MPa	2.41	4.28	2.65	3.46	2.42	2.87	2.78
Tensile Strength, MPa	5.79	8.61	4.92	7.23	5.61	5.41	4.74
Ultimate Elongation, %	441	477	402	496	426	440	364
Toughness, MJ/m ³	15.7	27.3	13.5	23.5	14.8	16.4	12.1
Tension Set, 100 % elongation, 10 minutes, room temperature							
% Set	8.5	16.0	10.0	12.0	8.5	9.5	9.5
Compression Set, 22 hours							
% Set @ 100C	28.9	38.3	42.0	37.4	27.0	39.0	39.1
% wt. gain							
% Swell @ 125C	96.3	75.5	128.9	112.0	94.1	130.5	121.2
% Swell @ 100C	80.3	59.2	115.0	84.6	80.8	110.3	108.6

Table IX

Physical Properties of TPV Blends with Non-Metallocene Polypropylene Copolymers					
	41C	42C	43C	44C	45C
TPV-1	100	100	100	100	100
Escorene PD9272		3.34	13.4		
Escorene PD 7032				3.34	13.4
PP:PP Copolymer Ratio	100:0	100:25	100:100	100:25	100:100
Final Brabender Torque	361	350	320	345	340
Physical Properties, Unaged					
Hardness, Shore A	63	81	76	67	78
50 % Modulus, MPa	1.70	2.02	2.99	2.00	3.08
100 % Modulus, MPa	2.38	2.73	3.74	2.71	3.83
Tensile Strength, MPa	5.92	6.12	8.50	6.06	7.34
Ultimate Elongation, %	462	449	531	438	451
Toughness, MJ/m ³	16.6	17.4	28.3	16.8	22.6
Tear Strength (N/mm)	22.28	26.71	36.42	25.32	33.76
Tension Set, 100 % elongation, 10 minutes, room temperature					
% Set	7.4	8.5	13.5	9.00	13.0
Compression Set, 22 hours					
% Set @ 100C	27.6	29.9	41.5	29.3	37.6
% Set @ RT	15.0	17.9	27.3	17.9	22.6
Weight Gain					
% Swell @ 125C	96.2	104.5	137.2	154.1	189.6
% Swell @ 60°C	65.0	60.6	49.20	57.2	50.5

[0049] Table X illustrates that the effect of the random propylene copolymers occurs in both TPV-1 (13.4 weight percent polypropylene) and TPV-2 (58.3 weight percent polypropylene).

[0050] Table XI compares 1) TPV-3 (9.4 weight percent polypropylene) with 2) TPV-3 with a random propylene copolymer and 3) TPV-1 which has 13.4 weight percent polypropylene. The toughness increase in examples 54 and 55 is a result of the random propylene copolymers rather than just the percentage polypropylene.

[0051] Table XII illustrates the effect of adding a random propylene copolymer before or after the curing (vulcanization) of the rubber phase.

[0052] Table XIII illustrates the effect of a random propylene copolymer on TPV's 4 and 5 which use nitrile rubber and butyl rubber respectively (rather than EPDM rubber as used in TPV-1 through 3 in the previous tables).

Table X

Physical Properties of Harder TPV Blends with Random Propylene Copolymers							
	46C	47	48	49	50	52	52
	avg. 4						
TPV-2	100.00	100.0	100.0	100.0	100.0	100.0	100.0
Expt M-PP D		11.2	24.9	43.9			
Expt M-PP C					11.2	24.9	43.9
PP:PP Copolymer Ratio	100:0	100:19	100:43	100:74	100:19	100:43	100:74
Final Brabender Torque	570	600	640	680	530	500	500
Physical Properties, Unaged							
Hardness, Shore D	55.5	55	54	53	53	50	44
50 % Modulus, MPa	15.1	14.7	14.1	13.0	13.1	10.8	9.03
100 % Modulus, MPa	14.5	14.1	13.5	12.7	12.7	10.8	9.44
Tensile Strength, MPa	16.9	22.0	26.3	27.6	18.1	19.9	20.4
Ultimate Elongation, %	438	586	715	725	545	678	700
Toughness, MJ/m ³	64.9	91.0	119.6	117.8	75.3	89.2	87.2
Tension Set, 100 % elongation, 10 minutes, room temperature							
% Set	60.5	58.0	59.5	48.0	54.5	48.5	39.5

Table Xi

Effect of Random Propylene Copolymer on TPV-3 and Comparison to TPV-1				
	53C	54	55	56C
TPV-3	100.00	100.0	100.0	
TPV-1				100.00
Expt M-PP D		6.4	13.6	
PP:PP Copolymer Ratio	100:0	100:68	100:144	100:0
Final Brabender Torque	240	250	275	380
Physical Properties, Unaged				
Hardness, Shore A	34	41	48	62
50 % Modulus, MPa	0.57	0.86	1.08	1.68
100 % Modulus, MPa	0.94	1.30	1.55	2.34
Tensile Strength, MPa	2.64	4.31	6.30	5.71
Ultimate Elongation, %	429	586	730	451
Toughness, MJ/m ³	6.8	14.7	24.8	15.8
Tension Set, 100 % elongation, 10 minutes, room temperature				
% Set	5.0	6.50	7.00	8.00
Compression Set, 22 hours				
% Set @ 100C	21.2	29.9	36.7	27.6
Weight Gain				
% Swell @ 125C	133.7	178.5	239.8	95.1
% Swell @ 60C	93.5	87.9	72.6	59.9
Tear Strength (N/mm)	10.81	17.29	23.26	22.35

Table XII

Effect of Adding Random Propylene Copolymer before or after Vulcanization								
	57C	58	59	60C	61	62	63	64
TPV-1	100.0	100.0	100.0	100.0	100.0	100.0	100.0	100.0
Expt M-PP C		13.3	13.3					
Expt M-PP E							13.3	13.3
Expt M-PP D					13.3	13.3		
Mixing temp °C	175	175	175	175	175	175	175	175
PP Copolymer/ Addition Sequence	N/A	before cure	before cure	N/A	before cure	after cure	before cure	after cure
PP Copolymer Concentration wt. %	0%	11.8	11.8	0	11.8	11.8	11.8	11.8
PP:PP Copolymer Ratio	100:0	100:100	100:100	100:0	100:100	100:100	100:100	100:100
Final Brabender Torque	440	320	380	400	420	530	310	350
Physical Properties								
Hardness, Shore A	N/A	N/A	N/A	59	70	68	71	70
50 % Modulus, MPa	1.6	1.4	1.4	1.5	2.3	2.3	2.5	2.3
100 % Modulus, MPa	2.5	2.0	2.0	2.2	3.1	3.1	3.2	3.2
Tensile Strength, MPa	4.7	3.6	4.2	4.5	6.9	7.4	6.4	7.1
Toughness, MJ/m ³	7.6	7.6	9.0	8.8	18.3	19.5	17.3	18.2
Ultimate Elongation, %	265	316	339	311	426	438	416	412
Oil Swell, 24 hrs at 125C	87.8	123.4	135.2	117.0	158.5	167.7	135.5	152.3
Compression Set, 22 hours								
@ 100C, % Set	24.2	49.6	49.3	32.2	39.4	36.6	39.7	42.1
@ RT	13.7	21.1	22.2	16.8	21.0	18.3	20.8	20.5
Tear Strength	18.65	19.50	20.48	21.2	29.3	32.29	29.70	31.75
Tension Set, %	5.5	8.0	8.0	6.5	9.5	11.0	11.5	11.5

Table XIII

Physical Properties of blends of TPV and PP or PP Copolymer Where the TPV Rubber is Nitrile Rubber and Butyl Rubber					
	65C	66	67	68C	69C
Formulation, phr					
TPV-4	100.0	100.0	100.0	100.0	100.0
TPV-5					
Expt M-PPD		6	12		
Lyondell 51S07A				2	4
PP Copolymer Concentration	0.0%	5.7%	10.7%	0.0%	0.0%
PP:PP Copolymer Ratio	100:0	100:40	100:80	100:0	100:0
Rubber Type	Nitrile	Nitrile	Nitrile	Nitrile	Nitrile
Physical Properties, Ungaged					
Hardness, Shore A	69	71	74	71	73
50 % Modulus, MPa	2.39	2.89	3.07	2.94	3.20
100 % Modulus, MPa	3.36	3.85	4.01	3.97	4.29
Tensile Strength, MPa	5.58	7.51	9.15	6.44	7.03
Ultimate Elongation, %	219	283	335	232	236
Toughness, MJ/m ³	7.61	12.91	17.76	9.65	10.70
Tension Set, % set	8.5	12.0	14.0	9.5	11.0
	70	71	72	73C	74
Formulation, phr					
TPV-4					
TPV-5	100.0	100.0	100.0	100.0	100.0
Expt M-PP D		6	12		
Lyondell 51S07A				2	4
PP Copolymer Concentration	0.0%	5.7%	10.7%	0.0%	0.0%
PP:PP Copolymer Ratio	100:0	100:38	100:75	100:0	100:0
Rubber Type	Butyl	Butyl	Butyl	Butyl	Butyl
Physical Properties, Ungaged					
Hardness, Shore A	57	61	65	61	66
50 % Modulus, MPa	1.50	1.84	2.09	1.81	2.06
100 % Modulus, MPa	2.24	2.61	2.86	2.62	2.92
Tensile Strength, MPa	6.16	7.44	8.30	6.46	7.11
Ultimate Elongation, %	343	386	410	336	348
Toughness, MJ/m ³	11.33	15.41	18.22	12.28	14.15
Tension Set, % set	7.5	10.0	12.0	9.5	11.0

[0053] While in accordance with the patent statutes the best mode and preferred embodiment has been set forth, the scope of the invention is not limited thereto, but rather by the scope of the attached claims.

Claims

1. A thermoplastic vulcanizate composition, comprising;

from about 20 to about 85 parts by weight rubber and from about 15 to about 80 parts by weight total of semi-crystalline polypropylene and a random propylene copolymer wherein said parts by weight are based upon 100 parts by weight of said rubber, said random propylene copolymer, and said polypropylene.
 wherein the weight ratio of said polypropylene to said random propylene copolymer is from about 100:2 to 100:400 and wherein said random propylene copolymer has a heat fusion of less than 75 joules/gram and comprises from about 80 to about 95 weight percent repeat units from propylene and from about 5 to about 20 weight percent of repeat units from one or more other unsaturated olefin monomers having 2 or from 4 to 12 carbon atoms based upon the weight of said random propylene copolymer,
 wherein said rubber comprises an ethylene-propylene-diene rubber, natural rubber, butyl rubber, halobutyl rubber, halogenated rubber copolymer of p-alkylstyrene and at least one isomonoolefin having 4 to 7 carbon atoms, a copolymer of isobutylene and divinyl-benzene, a rubber homopolymer of a conjugated diene having from 4 to 8 carbon atoms, or a rubber copolymer having at least 50 weight percent repeat units from at least one conjugated diene having from 4 to 8 carbon atoms or combinations thereof.

A thermoplastic vulcanizate composition, comprising;

from about 20 to about 85 parts by weight rubber and from about 15 to about 80 parts by weight total of semi-crystalline polypropylene and a random propylene copolymer wherein said parts by weight are based upon 100 parts by weight of said rubber, said random propylene copolymer, and said polypropylene.
 wherein the weight ratio of said polypropylene to said random propylene copolymer is from about 100:2 to 100:400 and wherein said random propylene copolymer comprises from about 80 to about 95 weight percent repeat units from propylene and from about 5 to about 20 weight percent of repeat units from one or more other unsaturated olefin monomers having 2 or from 4 to 12 carbon atoms based upon the weight of said random propylene copolymer,
 wherein said rubber comprises an ethylene-propylene-diene rubber, natural rubber, butyl rubber, halobutyl rubber, halogenated rubber copolymer of p-alkylstyrene and at least one isomonoolefin having 4 to 7 carbon atoms, a copolymer of isobutylene and divinyl benzene, a rubber homopolymer of a conjugated diene having from 4 to 8 carbon atoms, or a rubber copolymer having at least 50 weight percent repeat units from at least one conjugated diene having from 4 to 8 carbon atoms or combinations thereof.

3. A composition according to claim 2, wherein said rubber was dynamically vulcanized in the presence of said semi-crystalline polypropylene or the random propylene copolymer or both, thereby forming said thermoplastic vulcanizate.

A composition according to claim 3, wherein said random propylene copolymer has a peak melting temperature between about 25°C and about 105°C.

5. A composition according to claim 4, wherein one or more olefin monomers comprises from about 5 to about 20 weight percent repeat units from at least one olefin having from 2 or 4 to 8 carbon atoms.

6. A thermoplastic vulcanizate composition according to claim 4, wherein said peak melting temperature is from about 30 to about 105°C.

7. A composition according to claim 4, wherein said peak melting temperature is from about 40 to about 100°C.

8. A composition according to claim 6, wherein said semi-crystalline polypropylene has a melting temperature of at least 120°C and said composition further includes at least one oil, at least one filler, and at least one other additive.

9. A composition according to claim 6, wherein said random propylene copolymer comprises from about 80 to about 95 weight percent repeat units from propylene and from about 5 to about 20 weight percent repeat units from at least one monoolefin having from 2 or 4 to 8 carbon atoms.

10. A composition according to claim 6, wherein said random propylene copolymer comprises from about 80 to about 90 weight percent repeat units from propylene and from about 10 to about 20 weight percent repeat units from at

least one monoolefin having from 2 or 4 to 8 carbon atoms.

11. A composition according to claim 2, wherein said rubber comprises ethylene-propylene-diene rubber.

5 12. A composition according to claim 2, wherein said rubber comprises butyl rubber, halobutyl rubber, or a halogenated rubber copolymer of p-alkylstyrene and isobutylene.

13. A composition according to claim 2, wherein said rubber comprises natural rubber.

10 14. A composition according to claim 2, wherein said rubber comprises a rubber homopolymer of a conjugated diene having from 4 to 8 carbon atoms or a rubber copolymer having at least 50 weight percent repeat units from at least one conjugated diene having from 4 to 8 carbon atoms or combinations thereof.

15. A process for making a thermoplastic vulcanizate composition, comprising:

15

blending in any order

a) a rubber,

b) semi-crystalline polypropylene, and

c) a random propylene copolymer said rubber being from about 20 to about 85 parts by weight rubber, the total weight of said semi-crystalline polypropylene, and said random propylene copolymer being from 15 to 80 parts by weight, wherein said parts by weight are based upon 100 parts by weight of said rubber and said semi-crystalline polypropylene, and a said random propylene copolymer, wherein the weight ratio of said polypropylene to said random propylene copolymer is from about 100:2 to 100:400 and wherein said random propylene copolymer comprises from about 80 to about 95 weight percent repeat units from polypropylene and from about 5 to about 20 weight percent of repeat units from one or more other unsaturated olefin monomers based upon the weight of said random ethylene copolymer, and

25

30

dynamically vulcanizing said rubber after blending with said semi-crystalline polypropylene, or said random propylene copolymer, or combinations thereof.

16. A process according to claim 15, wherein said random propylene copolymer has a peak melting temperature from about 25 to about 105°C.

35

17. A process according to claim 15, wherein said random propylene copolymer has a peak melting temperature from about 30 to about 105°C.

18. A process according to claim 15, wherein said random propylene copolymer has a peak melting temperature from about 40 to about 100°C.

19. A process according to claim 15, wherein said random propylene copolymer is added and blended after said rubber is vulcanized.

45

20. A composition according to claim 2, wherein said composition has at least a 25 % increase in toughness and a less than 5 percent increase in modulus over a similar composition wherein the semi-crystalline polypropylene totally replaces the combination of semi-crystalline polypropylene and random propylene copolymer.

50

21. A composition according to claim 2, wherein said random propylene copolymer comprises a first and a second random propylene copolymer with a weight ratio of said first copolymer to said second copolymer of from 95:5 to 5:95 wherein said first copolymer has a melting point above 70°C and said second copolymer has a melting point below 60°C.

55

22. A composition according to claim 2, wherein said composition has at least a 25 percent reduction in tension set after 100 percent elongation for 10 minutes at 23±2°C over a similar composition wherein the semi-crystalline polypropylene totally replaces the combination of semi-crystalline polypropylene and random propylene copolymer.



European Patent
Office

EUROPEAN SEARCH REPORT

Application Number
EP 99 11 2169

DOCUMENTS CONSIDERED TO BE RELEVANT			
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int.Cl.7)
X	WO 98 27155 A (ADVANCED ELASTOMER SYSTEMS ; EXXON CHEMICAL PATENTS INC (US)) 25 June 1998 (1998-06-25)	2,3,11, 15	C08L23/10 C08L21/00
Y	* page 7, line 12 - page 10, line 5; examples 57,61 *	1,4-10, 12-14, 16-22	
Y	WO 98 27154 A (ADVANCED ELASTOMERS/EXXON) 25 June 1998 (1998-06-25)	1,4-10, 12-14, 16-18, 20-22	
Y	* page 12, line 9 - page 14, line 11; tables III, V * * page 7, line 17 - page 9, line 30 * * page 2, line 25 - page 3, line 26 *		
Y	US 4 247 652 A (MATSUDA AKIRA ET AL) 27 January 1981 (1981-01-27)	19	
	* column 5, line 22 - line 35 * * column 6, line 17 - line 25 *		
A	EP 0 794 226 A (MITSUI PETROCHEMICAL IND) 10 September 1997 (1997-09-10)	12,19	TECHNICAL FIELDS SEARCHED (Int.Cl.7) C08L
	* example 1 *		
The present search report has been drawn up for all claims			
Place of search THE HAGUE		Date of completion of the search 27 September 1999	Examiner Schmidt, H
<p>CATEGORY OF CITED DOCUMENTS</p> <p>X : particularly relevant if taken alone Y : particularly relevant if combined with another document of the same category A : technological background O : non-written disclosure P : intermediate document</p> <p>T : theory or principle underlying the invention E : earlier patent document, but published on, or after the filing date D : document cited in the application L : document cited for other reasons & : member of the same patent family, corresponding document</p>			

EPO FORM 1503 03/92 (Pct/Co1)

**ANNEX TO THE EUROPEAN SEARCH REPORT
ON EUROPEAN PATENT APPLICATION NO.**

EP 99 11 2169

This annex lists the patent family members relating to the patent documents cited in the above-mentioned European search report. The members are as contained in the European Patent Office EDP file on
The European Patent Office is in no way liable for these particulars which are merely given for the purpose of information.

27-09-1999

Patent document cited in search report	Publication date	Patent family member(s)	Publication date
WO 9827155 A	25-06-1998	AU 5528698 A	15-07-1998
		AU 5608198 A	15-07-1998
		WO 9827154 A	25-06-1998
WO 9827154 A	25-06-1998	AU 5528698 A	15-07-1998
		AU 5608198 A	15-07-1998
		WO 9827155 A	25-06-1998
US 4247652 A	27-01-1981	JP 1290567 C	29-11-1985
		JP 54112967 A	04-09-1979
		JP 60011937 B	29-03-1985
		JP 1290568 C	29-11-1985
		JP 54120669 A	19-09-1979
		JP 60011938 B	29-03-1985
		JP 1112028 C	16-09-1982
		JP 53145857 A	19-12-1978
		JP 56015740 B	11-04-1981
		JP 1194276 C	12-03-1984
		JP 53149240 A	26-12-1978
		JP 56015741 B	11-04-1981
		JP 1112029 C	16-09-1982
		JP 53149241 A	26-12-1978
		JP 56015742 B	11-04-1981
		CA 1109978 A	29-09-1981
		DE 2822815 A	07-12-1978
		DE 2858770 C	23-06-1994
		FR 2392072 A	22-12-1978
		GB 1590240 A	28-05-1981
EP 0794226 A	10-09-1997	IT 1096340 B	26-08-1985
		NL 7805780 A, B,	28-11-1978
		US 4212787 A	15-07-1980
EP 0794226 A	10-09-1997	AU 705660 B	27-05-1999
		AU 1506297 A	11-09-1997
		CA 2198998 A	04-09-1997
		CN 1164544 A	12-11-1997
		DE 69700305 D	12-08-1999
		JP 9296063 A	18-11-1997
		US 5786403 A	28-07-1998